

## II. Specification Amendments

The present invention relates to a fluid-separating device, for separating fluid and/or fluid spray from a gas. ~~Such separators are for example applied~~ Fluid-separating devices may be used, for example, for separating oil or oil spray from blow-by gases (crank housing gases, blow-through gases) of combustion engines. A further scope of application for ~~fluid separators~~ lays fluid-separating devices is in the field of electrochemical cells, in particular PEM polymer electrolyte membrane (PEM) fuel cells, in particular those which operate in a temperature range suitable for H<sub>2</sub>O, in particular between 20°C and 160°C.

Such fuel cells typically have powers between a few watts and several kilowatts. Such PEM fuel cells (~~polymer electrolyte membrane fuel cells~~) have a polymer membrane permeable to protons. This membrane needs to have a certain determined moisture content in order not to dry out and thus not to lose its functioning ability on account of this. ability to function. For this reason, the supplied reaction gases are previously humidified. For this, according to the state of the art, treated water in a humidifier is used for the corresponding supplied reaction gases on the anode and cathode side.

On the other hand, on the cathode side of the fuel cells pure water arises is produced as a reaction product. Thus, so that here on the exit side an enormous water excess is present in the gases which are ~~led away~~ drained off. The water, which condense directly condenses immediately after leaving the fuel cell. In order to separate this water from the gases which are ~~led away~~ drained off, one likewise applies fluid separation

devices in order to lead back this water back for humidifying.

According to the state of the art, common labyrinths, or metal knitted fabrics, or in particular cyclones are used for separating fluid.

For separating dust particles from gases, tubular separators are known which comprise a flow-through tube through which the gas is led. Worms are arranged in the flow-through tube which force the gas onto a circular path (orbit) along the inner periphery of the tubes and in this manner separate the particles on the inner wall of the tubes.

One fluid separator in the form of an oil separator or oil spray separator is known from DE 101 27 820 A1. There, a tubular separator is used which has a diameter of more than 5 cm. Accordingly, only a coarse separation of the oil from blow-by gases is effected in this spiral flow path. For this reason, a further fine separation device follows this separation device.

Further known fluid separators in the form of tubular separators, as for by way of example, are described in the patent applications of the same applicant with the file application number DE 102004011176.6 and DE 102004011177.4, as well as corresponding international applications, filed on the same day as the present application by the same applicant, which claim the priority of these applications. Those separators consist of a base body through which flow-through tubes pass, and for each individual flow-through tube, of a worm-like segment (spiral insert) is placed into the

respective flow-through tube.

~~At the same time, as is usual in the technical language~~ Typically, a worm is defined as a helical, or also spiral thread ~~led~~ passing around a middle axis.

The length of the ~~introduced segments at the same time is directed to~~ depends on the conditions of installation and the demanded separation performance and is often a multiple of the pitch of the segment. A one-piece manufacture of such long segments together with the flow-through tubes, however, ~~comes face to face with~~ has great difficulties with regard to manufacturing technology and is even not possible for certain materials and manufacturing methods.

The base body, the flow-through tubes and the worm-like segments of the individual flow-through tubes are therefore separate or separately manufactured parts. ~~This necessitates~~ Therefore, the individual parts ~~having~~ have to be securely connected to one another. ~~Thus in~~ In particular the individual worm-like segments need to be secured in the respective flow-through tubes.

Since several small fluid separator elements in a base body have a better efficiency than one large fluid separator element, and since several small fluid separator elements may be better adapted to the respective task (e. g. to an oil quantity to be separated in a motor or to a water quantity to be separated in a fuel cell, to the conditions of installation and likewise), the trend towards a larger number of individual fluid separator

elements per base body or per fluid separation device continues.

It is the object of the present invention to provide a fluid separation device ~~with~~in which the number of parts is significantly reduced, wherein the fluid separation device ~~despite~~ this nevertheless may be manufactured in an ~~economic~~economical manner and with a low failure rate.

~~This is achieved by a fluid separation device according to claim 1 as well as by a manufacturing method according to claim 14. Advantageous designs are described in the respective dependent claims. The uses of such fluid separation devices are specified in the claims 16 and 17.~~

The fluid separation element according to the invention (and thus also the fluid separation device) belongs to the class of tubular separators since it is provided with a flow-through tube with an inlet and with an outlet for the gas.

The Therefore, the basis of the fluid separation device according to the invention as a result is a fluid separator element with a flow-through tube and a worm-like segment arranged therein.

According to the invention, it is characterised in that the flow-through tube and the worm-like segment have been manufactured as one piece, thus as a common joint fluid separator element.

These fluid separator elements are integrated into a plate-like base body, wherein their ~~now-through~~ flow through direction is advantageously essentially perpendicular to the plane of the plate of the base carrier. The individual fluid separator elements as well as the associated base carrier (base body) are designed as one piece, thus as a common joint component.

The individual segments ~~at the same time~~ have a length (in the axial direction) of less than 0.5 pitches. However, the ~~The~~ flow-through itself ~~however~~ including an inlet and/or outlet region may have a larger length. The pitch ~~as the same time~~ here is defined as the length of the worm-like segment in the axial direction of the passage which the segment were to have with a complete revolution of the thread surfaces (= screw surfaces) by 360°.

Since the worm-like segments have a length of ~~maximally~~ at the most up to half a pitch, each base carrier may be manufactured as one piece as a cast part, in particular as a die-cast or an injection moulded part. By way of this it becomes possible to manufacture the flow-through tube and the worm-like segment of a fluid separation element, or all fluid separation elements and their base carriers in the same manufacturing cycle. Thus many flow-through tubes may be manufactured in a ~~passage~~ single work step with an integrated worm-like segment in the same subject. Very small inner diameters for the flow-through tubes, for example 3 mm, are possible ~~on account~~ as result of this method.

In one advantageous embodiment, at least two base carriers manufactured in such a manner are arranged bordering one another such that the individual fluid separator elements (or their flow-through tubes) of the individual base carriers are allocated to one another such that in each case one fluid separator element or flow-through tube of a base carrier, with the associated fluid separator element or flow-through tube of the at least one adjacent base carrier, forms a common flow path for the gas, said the flow path reaching through all base carriers arranged on one another.

It is particularly advantageous when ~~at the same time~~ the rotational direction (clockwise or anticlockwise~~counterclockwise~~) of the gas which is produced by the worm-like segments changes between two base carriers arranged adjacent to one another: if a first segment has a counterclockwise ~~an anti-clockwise~~ rotational direction of the thread surfaces of the worm-like segment in the gas flow direction, then the subsequently arranged worm-like segment has a clockwise rotational direction of the thread surfaces or of the associated flow path or paths.

It has now been surprisingly ascertained that with such a serial arrangement of at least two such fluid separator segments, in which (so that a common flow path for the gas is formed ~~from~~ by the flow-through tubes and worm-like segments of individual fluid separator elements of base carriers arranged one after the other,) ~~of at least two such fluid separator segments wherein~~ the individual segments advantageously ~~maximally~~ have a length corresponding to at the most 0.5 times their pitch, the separation may be

carried out in an extremely efficient manner. This is, also and indeed especially the case when the rotational direction of successive segments is in opposite directions to one another, so that the gas must be deflected from the one rotational direction to the other rotational direction within the serially connected flow-through tubes of two fluid separator elements.

~~By way of~~ With these worm-like segments being serially connected serially with an opposite rotational direction, impingement surfaces arise on which the fluid or the fluid spray is separated in an excellent manner. The thread surfaces of the worm-like segments may ~~at the same time~~ also be arranged such that the thread surfaces of the subsequent segment project into the flow path formed by a thread surface of the preceding segment. ~~At the same time~~ Moreover, it is particularly advantageous if the thread surface of the first segment projects roughly up to the middle[[\*]] of and into the flow path formed by the thread surface of the second adjacent segment.

However, base carriers with segments which are aligned in the same direction may be arranged bordering adjoining one another.

The outlet-side outlet-sided edge of a first segment and the inlet-sided edge of the subsequently arranged second segment, said the edges being arranged adjacent one another, may advantageously be arranged rotated (twisted) relative to one another about the central axis of the common flow path by an angle, in particular by an angle between 45° and 135° particularly preferred by about 90°.

Thus, with the first-mentioned fluid separation device, the rotational direction of the segments (spirals) changes in each case between adjacent base carriers. Therefore Thus for the complete separator unit it is sufficient to serially assemble only two base carriers reversed in rotational direction, in order to achieve a high separating performance for the gas flow on account of the change in rotational direction or the impingement surfaces which they entail respectively. Thus, irrespective irrespective of the number of base carriers arranged one after the other, thus the whole fluid separation device may be constructed merely from two different types of base carriers carrier. With Where there are lower demands with respect to the separation performance, or for the application as a coarse separator, one may also use only one plate-like base carrier.

Advantageously each of the separator elements has at least two flights or flow paths. For this, the flow-through tube is subdivided perpendicularly to the longitudinal axis in a manner such that two or more flights which are separate from from one another arise. For this a thread surface of one segment is sufficient. However[[, also]] the arrangement of several interwoven thread surfaces is also possible[[, too]].

In a further advantageous embodiment at least one of the flow paths has a smallest minimum cross section between 1 mm<sup>2</sup> and 800 mm<sup>2</sup>. It is particularly advantageous if such a flow path has a smallest minimum cross section of  $\geq 2$  mm<sup>2</sup> and/or  $\leq 400$  mm<sup>2</sup>, preferably  $\geq 4$  mm<sup>2</sup> and/or  $\leq 200$  mm<sup>2</sup>.

It is Advantageously advantageous that at least one flow path runs at an angle of about 45° to the axial direction. Advantageously Preferably, at least two of the successive consecutive, worm-like segments of the fluid separation devices adjacent to one another-are arranged directly connecting to one another or have with a positive-fit in the axial direction. The segments may however not be, however, arranged over the whole flow-through tube, but only at the beginning, in the middle and at the end of a flow-through tube. In the latter case thus also adjacent segments may be arranged somewhat separated from one another in the axial direction.

The flow may enter into the flow-through tube axially, or under certain circumstances also tangentially, and may exit this the tube axially and/or tangentially. An entry and exit at a limited angle with respect to the axial direction and/or the tangential direction is possible. However, from a technical point of view, an axial entry and/or exit of the gases is technically advantageous.

Advantageously, the inlet of the flow-through tube is arranged in a manner such that the flow-through tube has an inflow at an angle  $\leq 45^\circ$  to the axial direction or at an angle of  $\leq 45^\circ$  to the tangent on the periphery of the flow-through tube. Advantageously, the outlet is arranged in a manner such that the gas flows out of the flow tube at an angle  $\leq 45^\circ$  to the axial direction or at an angle  $\leq 45^\circ$  to the tangent on the periphery of the flow-through tube.

Flow-through tubes and/or flow paths arranged next to one another advantageously have the same diameter and thus the same pressure drop over the length of the flow-through tube or the flow path. As shown in Fig. 2, the tubes may be arranged such that a wall of one of tubes forms a wall of another tube. More particularly, the tubes may be arranged such that only a part of a wall of one tube forms part of a wall of another tube.

Advantageously, at least one of the flow-through tubes at its thinnest location has an inner diameter  $\leq 30$  mm, ~~preferably  $\leq 25$  mm, preferably  $\leq 12$  mm, preferably  $\leq 7$  mm.~~ In a preferred embodiment, the inner diameter is  $\leq 25$  mm. In a more preferred embodiment, the inner diameter is  $\leq 12$  mm. In a most preferred embodiment, the inner diameter is  $\leq 7$  mm. Advantageously, a flow-through tube and/or a flow tube formed of several serially arranged ~~flow-through~~ flow-through tubes, at its thinnest location or on its entire length has an inner diameter of  $\geq 1$  mm, ~~preferably  $\geq 2$  mm and preferably  $\leq 10$  mm.~~ In a preferred embodiment, the inner diameter is  $\geq 2$  mm and  $\leq 10$  mm.

In a further advantageous embodiment, the wall thickness of the thread surface of a segment at its thinnest location or on its entire length is more than 1/20 and/or less than half, advantageously more than 1/10 and/or less than 1/3 of the diameter of a flow-through tube or flow tube.

In a further advantageous embodiment, the pitch of a segment is  $\geq 1/8$ -fold and/or  $\leq 10$ -fold, advantageously  $\geq 1/4$ - and/or  $\leq 5$ -fold, advantageously  $\geq 1/2$  and/or  $\leq$  twice, the

diameter of the associated flow-through tube.

Further, The the flow-through tubes may be widened, advantageously further be conically widened, at the beginning and/or at their end, in order to minimise the pressure loss in the flow-through tube. A widening at the end of a flow-through tube furthermore reduces the gas speed so that at possible edges of the thread surfaces at the end of the last segment, no droplet shear and thus atomisation of the already separated fluid is effected.

~~One or more successive segments and/or the common flow tube formed over the whole length by way of the arrangement may be reduced in sections or over the whole length with respect to the diameter. The diameter of one or several consecutive segments and/or of the flow tube assembled to its final length may alter in sections or over the entire length.~~

In another embodiment, a segment of a fluid separation element (or also several or all serially arranged segments of the fluid separator elements associated with one another, of the serially arranged base bodies) in the axial direction, at the beginning and/or at the end has a thickened axial core of the segment or segments or end segments, said the core being thickened in a conical manner towards the beginning or end.

In a further embodiment for at least one of the segments or for several or all serially arranged segments of a common flow tube, the distance between the core of the worm-

like segment or the worm-like segments and the wall of the flow tube reduces in the axial direction.

In a further advantageous embodiment for one segment or for several or all serially arranged segments of a common flow tube, the radius of the core of the worm-like segment or of the worm-like segments and/or the diameter of the flow-through tube or of the common flow tube reduces in the axial direction.

In a further embodiment for at least one segment or for several or all serially arranged segments of a common flow tube, the pitch within the segment or the segments at least in sections increase-increases or reduces in the axial direction.

In a further advantageous embodiment, also at least the flow-through tube of a fluid separator element, or a common flow tube of fluid separator elements arranged serially, as an inlet region, may comprise a starting section and/or as an outlet region an end section, in which no worm-like segments are arranged.

Such a starting or end section advantageously has a length of greater more than double twice the diameter of the flow-through tube.

The individual base carriers may advantageously be designed as a flat plate (for example in a cylinder-shaped manner). Basically their shape is deduced from the installation situation with its spatial conditions and may be selected in an infinite

manner. The height of the plate (in the direction of the axial direction of the flow-through tubes of the individual fluid separator elements) is then advantageously less than about 1.5 times, preferably less than once and very particularly preferred less than 0.5 times the pitch of the worm-like segments of the individual fluid separator segments.

If several base carriers are arranged serially then it is advantageous if this is effected in a positive fit manner to one another. ~~For this~~ In this case, the base carriers may be connected to one another, for example glued, screwed and/or locked. In order to fix the relative position of the base carriers to one another, it is advantageous to design the base carriers in a manner such that they comprise means with which the relative position of two base carriers arranged adjacent to one another is defined relative to one another. This may ~~for example~~ be effected for example by way of tongue and groove elements and the like, which are provided ~~of~~ sides on surfaces of successive base carriers, ~~said sides~~ where the surfaces face one another. ~~said surfaces facing one another~~. It is also possible to provide the base carrier with a bore which ~~goes~~ passes through all base carriers, into which an arbor may be introduced. The bore and the arbor may, for example, likewise have tongues and grooves which then determine the position of the individual base carriers.

The base carriers for their part may be fastened via rails in the component surrounding them, for example in a water separator in a fuel cell or a valve cover for a combustion engine, wherein the size and arrangement of the rails is selected such that in each case one rail receives a base carrier with one of its edges. In this manner, by way of the

arrangement of the individual rails, the number of the base carriers as well as their relative position may likewise be fixed. Such a rail system further contributes to the modularity of the present invention.

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In order to ~~lead away~~ drain off the fluid separated at the wall of the serially connected flow-through tubes, their wall, advantageously in the axial direction may comprise grooves and channels. It is also possible in the axial direction to attach webs for leading the separated fluid to the outlet of the flow-through tube. The thread surfaces ~~tee~~ may as well comprise slots and/or channels which ~~lead away~~ drain off the separated fluid. It is particularly favourable if the grooves run in the outer edges of the thread surfaces.

The fluid separation device according to the invention has a series of advantages:

- the number of the required individual parts for the fluid separation device (worm-like segments, flow-through tubes or fluid separator elements) may be significantly reduced[[.]] ;
- this leads to considerable cost savings and simplification of the assembly[[.]] ;
- furthermore ~~the securing of the individual elements is done away with~~ can be dispensed with;
- the separation intensity is maximised in comparison to other cyclone-like separators. This particularly results when a multitude of fluid separator channels

(formed by at least one or by a plurality of fluid separator elements arranged serially and allocated to one another) operate in a parallel manner to one another[[.]] :

- ~~thus-a~~ compact, integrated fluid separation device with a low pressure loss, a high capacity and stable gas flows is provided-possible[[.]] ;
- the number of the individual flow-through tubes or common gas flow paths may be selected depending on e. g., the conditions within a fuel cell, where more water occurs on the cathode side than on the anode side, on the blow-by characteristics of a motor, on the maximal pressure drop and/or the maximal permissible fluid transfer.

If the flow-through tubes have a diameter  $\leq 30$  mm, then these may also be installed into flat valve bonnets (valve covers). With fuel cells there exists significantly more possibilities of incorporation so that no ~~such~~ extreme limitations with respect to the dimensioning are required.

The core (heart) of the worm-like segment may furthermore be removed in the inlet and/or in the outlet region, in particular with the (seen in the gas flow direction) first and/or last flow-through tube of a flow path. A further reduction of the flow pressure losses is effected by way of this. A cone-like removal of the core is particularly favourable so that a free flow region is present in the middle axis of the segment or the serially connected segments.

A few examples of the present invention are described in the following. Here, as in the following, the same or similar reference numerals are used for the same or similar elements so that the description to some extent is not repeated.

There are shown in:

- Figure 1 a cylinder head cover with installed oil separators;
- Figure 2 a section through a cylinder head cover;
- Figure 3 an oil separator with 2 base carriers;
- Figure 4 two base carriers together with integrated fluid separator elements for forming an oil separation device according to the invention;

Figures 5 and 6 the plan view in the axial direction of the base carrier according to Fig. 4;

- Figure 7 various shapes of worm-like segments;
- Figure 8 an oil separation device with two base carriers in a perspective view and a plan view as well as two worm-like segments of two oil separator elements, said the segments bordering one another and arranged serially in a common flow tube; and
- Figure 9 an electrochemical cell with a fluid separation device; and
- Figure 10 a single base carrier with integral fluid separator elements.

Figure 1 shows a cylinder head cover 1 which may be attached onto a cylinder head of a combustion engine. This cylinder head cover 1 comprises a cavity 2 which has an inlet 3 and an outlet 4 for gases. Now the The blow-by gases via the inlet 3 are blown

out of the crank case of the combustion engine into the cavity 2 and leave this cavity 2 via the outlet 4. The crank case gases are freed from entrained oil or oil spray within this cavity 2. This oil spray or the separated oil is collected in a siphon 6 and led back continuously into the oil sump or is also led back in portions.

Impingement plates 5 are arranged in the cavity 2 of the cylinder head cover 1 directly behind the inlet 3. ~~These impingement plates have the effect that a coarse separation of oil droplets is already effected on them. The impingement plates effect a coarse separation of oil droplets.~~ The impingement plates 5 ~~for this~~ are arranged offset such that a labyrinth-like path of the gas through the impingement plates results.

A separation device 10 according to the invention is arranged in the gas path behind the ~~oil~~-coarse separator of the impingement plate 5 and this device consists of two individual elements [[10a]] 10A and [[10b]] 10B. Each of the elements [[10a]] 10A and [[10b]] 10B comprises a plate-like base carrier [[21a]] 21A and [[21b]] 21B respectively~~[[,]]~~. ~~in each of which in each case at least one separator element 20a, 20b which may be recognised in cross section is arranged. In each element 10A, 10B, at least one separator element 20A, 20B is arranged.~~ Fig. 1 depicts the elements 20A, 20B in cross-section. The base ~~carriers~~ carrier [[21a]] 21A and [[21b]] 21B are fastened in rails which are formed in the housing of the cylinder head cover 1. The separator elements [[20a]] 20A and [[20b]] 20B ~~in each case~~ comprise a flow-through tube [[22a]] 22A, [[22b]] 22B ~~in each of which in each case a worm-like segment~~ [[23a]] 23A and [[23b]] 23B, respectively, is arranged. The blow-by gases enter into the flow-through

tubes [[22a]] 22A and [[22b]] 22B and are set into a rotating movement by way of the worm-like segments [[23a]] 23A and [[23b]] 23B. By way of this, the oil, or the oil spray, is spun out of the gas and is separated on the wall of the flowthrough flow-through tube [[22a]] 22A and [[22b]] 22B. The oil which is separated in this manner is transported along the wall of the flow-through tube [[22a]] 22A and [[22b]] 22B in the gas direction and subsequently runs into the siphon 6. Within the cylinder head cover, the flow-through tubes [[22a]] 22A and [[22b]] 22B at the same time represent the only (single) passage between the inlet and outlet 4 for the blow-by gases.

As is to be recognised in Figure 1, the worm-like segment [[23a]] 23A is installed and fixed in a rotated manner such that the gas is set into a clockwise rotational movement (clockwise direction). The segment [[23b]] 23B arranged after this has a rotational direction in the other direction so that there the rotational direction of the gas is reversed into a counterclockwise ~~an anticlockwise~~ rotation (opposite to clockwise direction). In particular, on account of such a reversal of the rotational direction, there results a particularly good separation rate of the separation device 10 represented here. It must be noted that the worm-like segments do not rotate themselves, but are fixed within the flow-through tubes.

Figure 2 shows a corresponding cylinder head cover 1 in a cut-out, wherein here a cavity 2 is likewise arranged in the valve cover 1, and in which a separation device 10 is likewise located. A siphon 6 for collecting the separated oil is likewise arranged after the impingement plates 5 and the separation device 10 in the gas flow direction.

From ~~this figure 2 it is now to be easily~~ can be recognised how the separation element 10 is constructed of two plate-like base carriers [[21a]] 21A and [[21b]] 21B. The two base carriers [[21a]] 21A and [[21b]] 21B are arranged in rail-like holders [[7a]] 7A, [[7a']] 7A' and [[7b]] 7B, [[7b']] 7B', respectively. Each of the base carriers furthermore comprises three separator elements [[20a]] 20A arranged next to one another transversely to the gas flow direction, for the base carrier [[21a]] 21A and as well as [[20b]] 20B, [[20b']] 20B' and [[20b"']] 20B" for the base carrier [[21b]] 21B. The further arrangement of the flow-through tubes [[22a']] 22A' and [[22b]] 22B, [[22b']] 22B' and [[22b"']] 22B" as well as the correspondingly marked worm-like segments [[23a]] 23A as well as [[23b]] 23B, [[23b']] 23B' and [[23b"']] 23B" corresponds to that of Figure 1. Here a reversal of the rotational direction of the gas flow between the base carriers [[21a]] 21A and [[21b]] 21B is also effected.

The worm-like elements, explained here with the example of the worm-like element [[23a]] 23A, have an inlet [[26a]] 26A of the flow-through tube [[22a]] 22A, an inlet-side edge [[29a]] 29A and as explained with the example of the flow tube [[22b]] 22B, an outlet-side edge [[30b]] 30B on an outlet [[27b]] 27B. The conditions in the other flow tubes correspond to these and therefore are not described separately.

In ~~this figure 3~~ it may be particularly well recognised that the outlet-side edge [[30a]] 30A of the separator element [[20a]] 20A and the inlet-side edge [[29b]] 29B of the separator element [[20b]] 20B are offset by 90° to one another, so that the inlet-side

edge [[29b]] 29B projects into the flow path of the gas of the separator element [[20a]] 20A. By way of this In this way, a particularly effective separation of oil and oil spray may be effected.

Figure 3 then shows two base carriers [[21a]] 21A and [[21b]] 21B of a separator device 10 as is for example used for example in Figure 2. Here, as in all previous and subsequent figures, similar or corresponding elements are indicated with similar or corresponding reference numerals (only modified by the additions such as A a, B b, ,"","). Here, it is to be recognised that the base carrier [[21a]] 21A and [[21b]] 21B are plate-like and the flow-through tubes [[22a]] 22A, [[22a']] 22A', [[22a'']] 22A'' etc. project from the respective base carriers [[21a]] 21A and [[21b]] 21B, respectively. The flow-through tubes contain worm-like segments, e. g. [[23b]] 23B, [[23b']] 23B', [[23b'']] 23B'',.... With regard to the invention, it is particularly advantageous that the respective base carrier [[21a]] 21A and [[21b]] 21B with the through flow tubes [[22a]] 22A, [[22a']] 22A',... and [[22b]] 22B, [[22b']] 22B',... arranged in it respectively, and the worm-like segments arranged in the respective flow-through tubes, may be manufactured as one piece for each base carrier [[21a]] 21A and [[21b]] 21B, respectively. This then may only be accomplished in an economical way and manner for example by way of injection moulding method or die casting method, for example, if the worm-like segments have a length which is smaller or equal to half a pitch of the respective worm-like element. Longer worm-like segments with regard to manufacturing technology would only be capable of being manufactured at an extremely great expense.

Figure 4 shows an oil separation device 10 which comprises two, in each case flat, cylinder-shaped base carriers [[21a]] 21A and [[21b]] 21B. The two base carriers [[21a]] 21A, [[21b]] 21B, for an improved representation, are sketched at a distance to one another in the direction of the axis of symmetry of the cylinder. In this oil separation device 10 according to the invention, the two plate-like base carriers [[21a]] 21A, [[21b]] 21B, however, are arranged directly bordering one another such that they form a common cylinder with a cylinder height which corresponds to the thickness of the two plate-like base carriers in the direction of the axis of symmetry. Four oil separator elements ([[20a]] 20A, ..., [[20b]] 20B, ...) with their flow-through tubes [[22a]] 22A, ..., [[22b]] 22B, ... together with the associated worm-like segments [[23a]] 23A, ..., [[23b]] 23B, ... are integrated into each base carrier [[21a]] 21A, [[21b]] 21B. The four oil separator elements [[20a]] 20A, ..., [[20b]] 20B, ... are arranged on a circle about the cylinder axis in the plane perpendicular to the cylinder axis. The worm-like segments [[23a]] 23A, ..., [[23b]] 23B, ... in each case have a length corresponding to half the pitch. Each base carrier [[21a]] 21A, [[21b]] 21B, its associated flow-through tubes [[22a]] 22A, ... and its associated worm-like segments [[23a]] 23A, ... is in each case manufactured as one piece as a common die-cast part. Both base carriers [[21a]] 21A, [[21b]] 21B by way of this may be integrated into a single oil separation device 10 in that the two cylinders [[21a]] 21A, [[21b]] 21B are arranged directly bordering one another in a manner such that the two cylinder axes coincide. At the same time then Then two flow-through tubes [[22a]] 22A and [[22b]] 22B or [[22a']] 22A' and [[22b']] 22B', in each of with one of the first base carrier [[21a]] 21A and one of the second base carrier [[21b]] 21B, form a common flow path for the gas. Thus, the flow-through tubes [[22a]]

22A and [[22b]] 22B together with their worm-like segments [[23a]] 23A and [[23b]] 23B form a common flow path. Since ~~then~~ all worm-like segments [[23a]] 23A, [[23a']] 23A',... of the one base carrier [[21a]] 21A have ~~an anticlockwise~~ a counterclockwise rotational direction and since all worm-like segments [[23b]] 23B of the other base carrier [[21b]] 21B have a clockwise rotational direction, and since the worm like segments [[23a]] 23A, [[23b]] 23B and [[23a']] 23A', [[23b']] 23B',... (of the different base carriers 21 and [[21b]] 21B), which are allocated to one another and which form a common flow path, are twisted to one another by 90° with respect to the central axis of the respective flow path 22, in the oil separation device 10 for each common flow path at the height of the transition from one into the other base carrier, ~~in each case a~~ an impingement surface is formed in each case which improves the separation of the oil.

In order to achieve ~~an exactly~~ exact fitting alignment of the two base carriers [[21a]] 21A, [[21b]] 21B in the oil separation device 10, the base carrier [[21b]] 21B on the surface which borders the other base carrier [[21a]] 21A is provided with a bulge 16 in the form of a cylindrical projection. This ~~projection~~ bulge 16 engages with a positive fit into a corresponding indentation (not shown) in the form of a cylinder-shaped recess into the base body [[21a]] 21A. The bulge 16 and the indentation serve for preventing a mutual rotation of the two base carriers [[21a]] 21A, [[21b]] 21B about the common cylinder axis in the completed assembled condition. The bulge 16 and the indentation thus serve to ensure the common flow paths through the oil separation device 10 and to fix the relative arrangement of the individual worm-like segments [[23a]] 23A, [[23b]] 23B of each individual common flow path.

In place of only one bulge 16 and associated indentation, embodiment examples with a plurality of lock-in possibilities ~~are possible~~ may be used. These embodiments, e. g., with a circular arrangement of an even number of worm-like segments with alternately arranged clockwise and counter clockwise rotating worm-like segments, offer the possibility of using the same basic modules for the manufacture of a fluid separator with a flow direction which is the same or ~~counter~~ inverse to one another, in the serially arranged worm-like segments.

If, for example, in Figure 4 in each case two separator elements [[20a]] 20A, [[20a']] 20A' which lie opposite one another are provided with worm-like segments [[23a]] 23A, [[23a']] 23A' which are in the same direction, for example clockwise, and the remaining separator elements [[20a"]] 20A" and 20 which lie opposite one another are provided with worm-like segments [[23a"]] 23A" and 23 which both are twisted ~~anti-clockwise~~ counterclockwise, then by way of serial arranging two such base carriers [[21a]] 21A one may effect any change in the rotational direction. This is because two base carriers may be arranged serially such that between them no change in the rotational direction in the respective separator elements is effected, or also by way of installing one of the base carriers offset by 90° such that a change in rotational direction between the serially arranged worm-like segments in the two base carriers is effected. The modularity may then be realised in a particularly simple manner if rails are arranged at the location of installation for serially arranged base carriers, in order to accommodate the carriers. By way of different orientation of the base carriers on insertion or

introduction into the corresponding rails one may then infinitely select which type of rotational direction and thus change in rotational direction between individual base carriers is to be effected.

Apart from an arrangement of successive worm-like segments 23, which alternate with respect to the rotational direction as in the introduced case, one may also arrange equally directed worm-like segments one after the other, wherein in both cases these are twisted relative to one another from base body to base body in each case by 90° about the central axis of the common gas flow path 22. Bores [[15a]] 15A, [[15b]] 15B are incorporated centrally into the cylinder-shaped base carrier [[21a]] 21A, [[21b]] 21B for aligning the cylinder axes of the base carrier. Guide pins may be introduced into these bores [[15a]] 15A, [[15b]] 15B in an exactly fitting manner.

The guide bores [[15a]] 15A, [[15b]] 15B may at the same time in each base body 9 be provided each with a fin (spring) in the direction of the cylinder axis. The corresponding guide pin may then have a notch or groove corresponding to this fin so that, by way of the guide pin one may achieve the desired positioning of the two base carriers [[21a]] 21A, [[21b]] 21B relative to one another with regard to the rotational position about the common cylinder axis. A tongue and groove may also be arranged on the respective other component in order to achieve the desired ~~rotational~~ ~~securement~~ anti-twist protection.

In the shown base carriers [[21a]] 21A, [[21b]] 21B, the axial directions of the individual

oil separator segments 20 or flow-through tubes 22 are directed parallel to the cylinder axis of the base carrier [[21a]] 21A, [[21b]] 21B. For achieving an inclination of the flow paths for ~~leading away~~ draining off fluid ~~also even~~ when the vehicle has been positioned obliquely, the complete oil separation device 10 may be installed tilted by an angle  $\alpha > 0^\circ$  to the horizontal (angle  $\alpha$  = angle between the central cylinder axis of the oil separation device and the horizontal). Alternatively ~~to this~~, the individual oil separator elements 20 may be integrated into the base carrier 21 in a manner such that the axial directions of the oil separator elements 20 form an angle  $> 0^\circ$  to the cylinder axis of the base carrier 21.

Figures 5 and 6 show views of the two sides of the base carrier [[21b]] 21B represented in Figure 4.

Figure 7, in part pictures 7A, 7B, and 7C, ~~in each case each show~~ shows worm-like segments 23 which all rotate clockwise (clockwise direction). One may recognise that these worm-like segments 23 comprise edges 30 on the inlet side and edges 29 on the outlet side. The worm-like segments 23 at the same time form two thread surfaces or thread surfaces [[28a]] 28A and [[28b]] 28B and divide the flow path of the gas into two flights. In the part figures A, B, C various variants are represented, wherein the inlet-side as well as the outlet-side bevelled edge 30 and 29 respectively are present in Figure 7A. The inlet-side edge in Figure 7B is designed differently, whilst in Figure 7C the outlet-side edge 29 and the inlet-side edge 30 have a different shape. Figure 7C, furthermore ~~in contrast to the Figures 7A and 7B,~~ has a stabilising core.

Figure 8 ~~sketches~~ depicts a view of two worm-like segments [[23a]] 23A and [[23b]] 23B as may be applied in a ~~common~~ joint flow path 25 by way of two base carriers of an oil separation device which are arranged one after the other. Both worm-like segments [[23a]] 23A, [[23b]] 23B have a length corresponding to 0.5 times their pitch as well as the same rotational direction (clockwise).

Figure 8 furthermore shows a cylinder-shaped separation device 10 in a lateral view in which two base carriers are integrated with a positive fit such that they are fixed to one another.

Figure figure 8 furthermore ~~sketches~~ depicts a plan view of the separation device 10 with a central guide bore 15 and at a different distance to this central guide bore, a plurality of oil separator elements [[20a]] 20A, [[20b]] 20B,....

Figure 9 shows a PEM fuel cell 40, which on the anode side, is supplied through a conduit 43 with fuel, for example, molecular hydrogen H<sub>2</sub>. The cathode-side reaction products are ~~led away~~ drained off via a conduit 42. The cathode-side reaction product is essentially H<sub>2</sub>O. With fuel cells, a humidification of the supply of fuel on the anode side through the conduit 43 as well as the cathode-side supply of fuel (O<sub>2</sub>, air or likewise) which here is not shown, is required, so that the membrane does not dry out and lose its function. For this, and shown by way of the example of the conduit 43, this conduit runs through a device for gas humidification. In this device, the anode-side fuel is

humidified.

On the other hand, on the cathode side (pure) water is produced as a reaction product so that an enormous excess of water is present in the conduit 42 at the exit side. This water which is ~~led away~~ drained off with the reaction gases via the conduit 42 may be removed from this waste gas. For this ~~then~~, according to the invention, a water separator device 10 is arranged in the conduit 42. Three base carriers [[21a]] 21A, [[21b]] 21B, [[21c]] 21C ~~which are~~ drawn by way of example contain water separator elements [[20c]] 20C, [[20c']] 20C' and [[20c"']] 20C" which are ~~likewise~~ drawn only in a ~~sketched manner~~ schematic form are located in this separation device. The separator elements in the base carriers [[21a]] 21A and [[21b]] 21B which are mounted upstream on the flow path of the gas, are ~~likewise~~ not shown here, but together with the separator elements [[20c]] 20C, [[20c']] 20C', [[20c"']] 20C" in each case form ~~common~~ joint flow paths. With such a separator the water droplets which condense indirectly after leaving the fuel cell in the conduit 42 may be separated.

Until now the water produced on the cathode side escapes into the outer air and expensively prepared water must be used in order to humidify the supplied reaction gases.

The pure water which in this manner is removed from the reaction gas may now however be led to the humidification device 41 via a water return conduit 44 so that no water needs to be supplied externally to the complete system in order to maintain the

circulation of water.

The base carriers 21A, 21B and the fluid separator elements 20A, 20B may be comprised of glass, plastic and/or metal. As a plastic, the base carriers 21A, 21B and the fluid separator elements 20A, 20B may be one or more of a thermoset, thermoplast and an elastomer with a  $T_g \geq 80^\circ\text{C}$ . The base carriers 21A, 21B and the fluid separator elements 20A, 20B may also be comprised of a polyamide material.

Finally, Figure 10 provides a depiction of the embodiment of the invention discussed above wherein a single base carrier is utilized by itself. For economy of description and to demonstrate the adaptability of the base carrier for use with another base carrier or for use by itself, the base carrier 21A discussed above and depicted in Fig. 4 is depicted alone. The base carrier 21A of Fig. 10 can be readily used in place of the two base carrier embodiments depicted herein by simply removing the second base carrier.